

AUTOMATA BASED MODELLING AND SIMULATION

Application in an Industrial Software Environment

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Abstract: Contemporary industrial systems are hybrid systems, and hybrid automata and Petri Nets are the most used approaches to model such systems. Despite academic efforts these two approaches did not meet wide acceptance when proposed for industrial use, mainly because they are application depended. In this paper, a recently proposed hyper-class of hybrid automata is presented, which seems to cover this weakness. Illustrating its use, an application of this new formulation method in an industrial software environment is given. The given example is taken from a chemical industry and uses PID controllers to control continuous variables, while the whole project was developed in a SCADA software platform.

1 INTRODUCTION

Most contemporary industrial systems are described as hybrid systems, since they are governed by discrete state controllers, whose internal state transitions are triggered by the value of some measured continuous physical quantity (temperature, flow rate, time, etc.). The importance of modelling and simulation of industrial production systems is generally acknowledged and hybrid automata (Antsaklis, 2000) and Petri nets (Peterson, 1981) are the most used approaches for modelling hybrid systems. But these methods did not meet wide acceptance when proposed for industrial use, primarily because they are application depended, or more accurate domain depended. A new automata-type method (Deligiannis, 2005) seems to avoid this dependence, offering the convenience of modelling various types of industrial systems without any restrictions on system's properties. It borrows some characteristics from several types of automata (Khoussainov, 2001), such as the control graph with a finite set of states and transitions between those states. It models hybrid systems handling both discrete and real valued variables combining flow, invariant and guard conditions from hybrid

automata, with clock constraints and delayed inputs from timed (Allur, 1994) and PLC automata (Dierks, 1997). In addition, introduces new modelling parameters as reset table at each transition and hierarchical classification of executable events at each state. Application independence derives from the fact that new method is a hyper-set of every other type of automata and hence is less application depended compared to any of them.

Apart from the used modelling method and despite huge advances in the field of control systems engineering, PID still remains the most common control algorithm in industrial use today. It is widely used because of its versatility, high reliability and ease of operation (Astron, 1995). PID systems' main advantage on applying control is that there is no need to obtain a dynamic model.

In this paper an example of industrial relevance is presented. A three tank system is modelled, using the new automata-type model, and implemented for simulation and verification in an industrial software environment. A PID controller was developed to control system's continuous dynamics. Implementation took place in CX – Supervisor, a *Supervisory Control And Data Acquisition* (SCADA) software by OMRON. Taking advantage of software's animation capabilities, screens

resembling real system were constructed in order to visualize system's operation.

2 THE HYPER – CLASS OF HYBRID AUTOMATA

This new hyper-class of hybrid automata was firstly introduced in (Deligiannis, 2005). Method's main aim is to bridge the gap between academic methods and real industrial applications, being suitable for modelling a large variety of industrial systems. It introduces new formulation parameters in addition with some of the conventional methods, and especially from the several types of automata.

Definition 1. We define an automaton by the 12-tuple:

$$A = \langle X, Z, Q, \Sigma, Init, Flow, L, S, W, E, R_X, R_Z \rangle.$$

Its structure is composed by the following sets:

- System's variables:
 - Real-valued variables: $X = \{x_1, x_2, x_3, \dots, x_m\}$
 - Discrete variables: $Z = \{z_1, z_2, z_3, \dots, z_k\}$
- Set of states: $Q = \{q_1, q_2, q_3, \dots, q_n\}$
- Alphabet or set of events: $\Sigma = \{\sigma_1, \sigma_2, \sigma_3, \dots, \sigma_\lambda\}$, which can be:
 - Discrete variables.
 - Conditions over the real-valued variables.
 - Any combination of them.
- Initial conditions: *Init*
 - $X = X_0, Z = Z_0$ and q_0
- Flow conditions:
 - $F(X, \dot{X}) = 0$
 - $Z_{i+1} = G(Z_i)$
- Invariant conditions: $L = \{\ell_1, \ell_2, \ell_3, \dots, \ell_n\}$
- Restrictions or safe values: $S = \{s_1, s_2, s_3, \dots, s_n\}$
- The set of events to be ignored until the satisfaction of restrictions: $W = \{w_1, w_2, w_3, \dots, w_n\}$ with $w_i \subseteq \Sigma$.
- Set of transitions: $E \subseteq Q \times Q \times \Sigma \times R_X \times R_Z$
- Reset table for each transition:
 - $X = R_X, Z = R_Z$

Each set $(q, q', \sigma, r_X, r_Z)$ represents a transition from state q to state q' , which is caused by the

event $\sigma \in \Sigma$. Set $r_X \subseteq R_X$ gives the real-valued variables to be resettled during this transition, while set $r_Z \subseteq R_Z$ gives the discrete variables.

As shown in figure 1, each state q_i has a corresponding set of parameters, which are:

- Flow conditions:
 - $F_i(X, \dot{X}) = 0$
 - $Z_{j+1} = G_j(Z_j)$
- Active events at present state: $\Sigma_i \subseteq \Sigma$. Set Σ_i has, by definition, ζ elements, each one of which belongs to set Σ . $\Sigma_i = \{\sigma_j^{i,k}\}$, where i is the present state, $k = 1, 2, \dots, \zeta$ and $j \in [1, \lambda]$. Index k also denotes transitions priority caused by different events. If two events occur simultaneously and cause two different transitions, transition with the lower index k will take place.
- Invariant conditions: ℓ_i
- Restrictions or safe values: s_i
- Set of events to be ignored until the satisfaction of restrictions: w_i

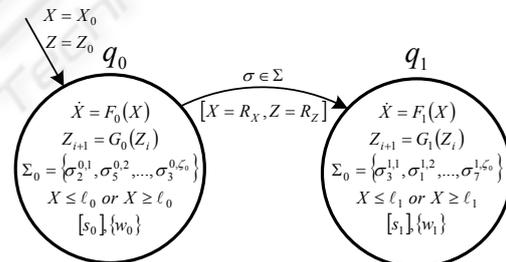


Figure 1: A simple automaton with two states.

3 A THREE TANK SYSTEM

Let us suppose an example from a chemical industrial procedure, which consists of three different tanks, as shown in figure 2. Tanks 1 and 2 contain two different liquid materials and both feed tank 3 simultaneous. The whole procedure starts through a start button. When start button is pressed, valves g and h open and both liquids flow to tank 3. Simultaneously, the mixing process starts by turning on the mixer p . There is a specific ratio between flows from tanks 1 and 2, according to the chemical procedure. Hence, at least one of the valves has to be controlled in order to meet procedure's

requirements. The controller used is PID, regulating flow from tank 2 and is described in the next section. When liquid's mass in tank 3 is 150 lt. both valves g and h close and the heating phase starts. Heating takes place by turning on heater k and stops when mixture's temperature arises to 600° C. At that time, mixer and heater turn off and valve j opens until tank 3 is empty.

Valve e is automatically controlled, so as to keep level in tank 1 between a and b . When level in tank 1 falls to b , valve e opens until level arises to a . Equivalently, valve f is controlled to preserve level in tank 2 between c and d limits.

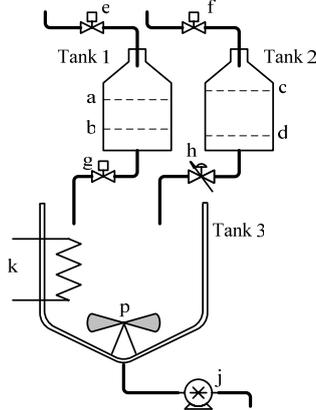


Figure 2: Example from chemical industry.

4 SUPERVISOR – SCADA ENVIRONMENT

SCADA is the acronym for Supervisory Control And Data Acquisition, a computer for gathering and analyzing real time data. SCADA systems are used to monitor and control a plant or equipment in industries. A SCADA system gathers information from the plant, transfers it back to a central site, carrying out necessary analysis and control, and displaying the information in a logical and organized fashion. SCADA systems were first used in the 1960s and since then, most of industrial engineers have become familiar with their use. This is the main reason for choosing CX – Supervisor as the software platform for illustrating the use of the new automata-type model, since this new method was presented with industrial orientation. In addition, CX – Supervisor comes with a Run-Time environment, where simulation of a system can take place.

The system, described in the previous paragraph, can be seen as wholeness, or in a different approach, as three independent subsystems, each one modelled

with a relative automaton. First two automata are very simple controlling tanks' inlet in accordance to liquids level. Third automaton is slightly more complex. It has a restriction in state q_1 , where event s_1 will be delayed until tank 1 is full ($a=1$). In addition states q_2 and q_3 have flow conditions according to which system's variables change their value. State q_3 has a flow condition giving temperature's rise until the upper limit of 600° C, when the heater is on. State q_2 implements the PID controller mentioned in the previous section in order to satisfy process criteria. More analytically, flow from tank 1 to tank 3 depends on liquid's level in tank 1 which fluctuates between a and b . Hence, the controller used has to adjust valve h so as to keep the desired rate between the two liquids' flow.

Based on these automata, a project was built in CX – Supervisor, a SCADA software environment by OMRON. A screen resembling automata's executions was developed. In this screen active state in each automaton turns red, while last transition is denoted with a green sign. Screenshots are depicted in figures 3 and 4.

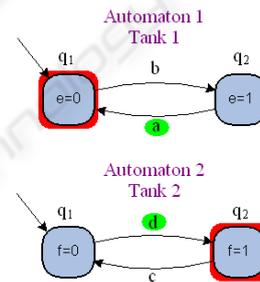


Figure 3: Screenshot of automata 1 and 2.

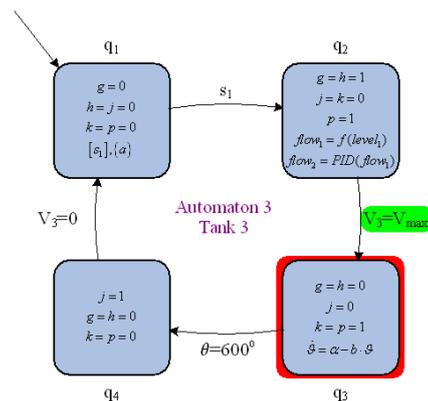


Figure 4: Screenshot of automaton 3.

Here, we have to mention that each state's components were reproduced by a script written at CX – Supervisor's embedded script editor in

accordance to the guide described in (Deligiannis, 2006). Due to software limitations and capabilities, differential equations were transformed to difference equations (Hamming, 1973). Especially for the controller, a PID algorithm given by SIEMENS was used. This algorithm calculates a particular manipulated variable increment dY_k at an instant $t = (k \times T_A)$ according to the following formula:

$$dY_k = K \cdot \left[(XW_k - XW_{k-1}) \cdot R + \frac{T_A}{T_N} \cdot XW_k + \frac{1}{2} \cdot \left(\frac{T_V}{T_A} \cdot (XW_k - 2 \cdot XW_{k-2}) + dD_{k-1} \right) \right]$$

At the instant t_k , manipulated variable Y_k is calculated as follows:

$$Y_k = \sum_{m=0}^k dY_m$$

Using the embedded features of our SCADA software, we have an overall supervision of our system. Data Log Viewer helps us test PID's operation since deviation from set point is measured and depicted on line. An operation example showing the percent of set point deviation is depicted in figure 5.

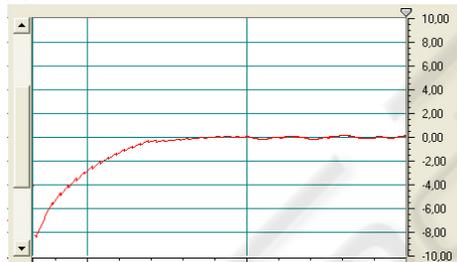


Figure 5: Percent of set point deviation.

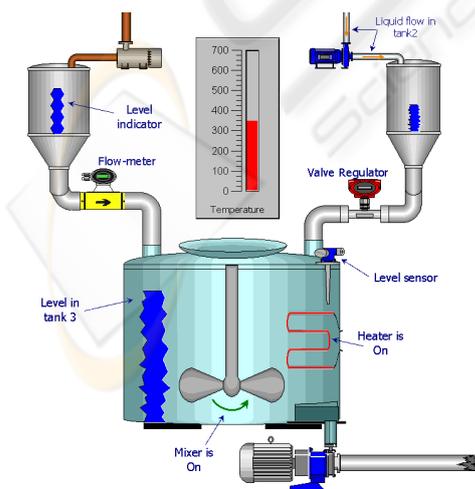


Figure 6: A screenshot from CX – Supervisor.

A SCADA software, just like CX – Supervisor, gives to the developer the opportunity to create screens resembling the real system. In figure 6, a screenshot of the project created, is shown. Each tank has the relative level indicator showing to the operator the liquid level inside the tank. The exact level is displayed in a relative table, where all system variables are shown. Taking advantages of software's animation capabilities, liquid flow is visualized as also mixer's movement.

5 CONCLUSIONS

A recently proposed automata-type method for modelling industrial systems was used in this paper illustrated through an example from a chemical industry. The given example was modelled and simulated in a SCADA software environment with run-time feature. Regarding future work on this field, one may have to examine if a model implemented in a SCADA software can be used not only for simulation but for control as well. A supervisor control station connected with a programmable logic controller would interact with a plant and control it.

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