# Particles from Volcanic Scoria Powders: Granulometry and Granulomorphology Data Analysis

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Abstract: This study presents size and shape parameters relevant to volcanic scoria powder characterization. Particle size distribution was compared using two different techniques, including laser diffraction and automated static image analysis, and their respective results were discussed. Specific information on particle shape has been obtained using image analysis by 2-D images. The image analysis was used to identify key controls on particle morphology, six shape parameters: elongation, circularity, solidity, roughness, bluntness and luminance have effectively accounted for the morphological variance of powder particles. The effect of the number of particles of testing samples on these variables obtained through the image analysis was investigated. To develop analytical models, Multiple linear regressions analysis was applied using the dataset. The dataset comprised size and shape information's about 24,268 particles from black natural powder, 32,302 particles from dark red natural powder, 22,562 particles from red natural powder and 25,041 particles from yellow natural powder. The analysis allowed us to identify the explanatory variables and develop eight mathematical models and three of these models are intended to prediction with very good significance. The correlation coefficients and analysis of variance test results obtained evidence the adequacy level of models. Thus, it is possible to estimate each dependent response parameter through the proposed models.

# **1 INTRODUCTION**

In the past few years, several studies have been published that focused on the characterization of maximum packing of supplementary cementitious materials (SCMs) in cement-based systems. The related works generally classified the factors that affect the matrix compactness into four groups: particle morphology, particle packing, interparticle spacing and matrix rheology (Felekoglu. 2009; Arvaniti et al, 2015a; Bouyahyaoui et al, 2018). Particle size and particle shape are closely related to the reactivity of SCMs. Industrial by-products, their partial replacement of cement in concrete mixes represents a substantial offset by the consequent environmental impact. The size and shape characterization of irregular particles is a key issue in many fields of science (Bagheri et al, 2015) and engineering (food, pharmaceutics, minerals, biology, astronomy, ...), which is often associated with large

uncertainties (Felekoglu. 2009; Bouyahyaoui et al, 2018; Bagheri et al, 2015; Liu et al, 2015; Dioguardi et al, 2018). The main characteristics of powders are the particle size (granulometry) and particle shape (morphology). Technological properties of powders depend on their granulometry and particle morphology (Pavlović et al, 2010).

To date, only a few studies have been published on particle size and particle shape parameters of mineral powders using as SCMs (Felekoglu. 2009; Bouyahyaoui et al, 2018; Bagheri et al, 2015; Hackley et al, 2004; Michel and Courard, 2014; Klemm and Wiggins. 2017). Technological properties of mineral powders (bulk density, flowability, surface area, etc.), as well as the potential areas of SCMs, depend on these characteristics (Mikli et al, 2001). It also has been known that powders may improve the particle packing density of cementitious system, and superplasticizers help to obtain the desired rheological properties by increasing the

workability without causing segregation in fresh state (Bouglada et al, 2019) and improve the mechanical properties and durability by reducing the water/cement ratio. Some of these powder materials are either industrial by-products or unprocessed materials. They provide environmental relief because industrial by-products are being recycled and hazardous emissions released into the atmosphere due to cement production are reduced, raw materials are preserved and energy is saved (Felekoglu. 2009). Besides, inert and semi-inert powders such as grounded volcanic scoria can be alternatively employed for high-performance mortar and concrete mixture designs (Juimo et al, 2017). More recent works have addressed the effects of volcanic scoria powder addition on rheological properties of cement paste (Bouglada et al, 2019; Tchamdjou et al, 2017a; Tchamdjou et al, 2017b).

Powders are problematic materials in the application of particle size analysis (Felekoglu. 2009). In general, sizing techniques work best over a limited size range. The optimum range of particle size analysis varies according to many factors, including detector sensitivity and the assumptions associated with the underlying principle of measurement (Felekoglu. 2009; Arvaniti et al, 2015b).

Most commercial methods are designed specifically for a range of particle size, and work best with homogeneous spheres. The degree to which irregularity affects the results vary with the technique employed, and is not well understood or exactly accounted for in many methods (Felekoglu. 2009; Bagheri et al, 2015; Orhan et al, 2004; Ferraris et al, 2002).

The morphology of raw powder includes its particle size distribution (PSD), specific surface area  $(S_{SB} \text{ or } S_{SL})$  and particle shape. The PSD can be determined by sieves analysis, laser diffraction (LD) and image analysis (IA). The industrial method to determine  $S_{SB}$  is Blaine Air Permeability test (Arvaniti et al, 2015a; Niesel. 1973). The evaluation of particle shape needs complex techniques such as the LD and the IA (Bagheri et al, 2015; Arvaniti et al, 2015b). Individual particle features should be captured by IA to derive the shape descriptors (Bouyahyaoui et al, 2018; Abazarpoor et al, 2017; Ilic et al, 2015).

In this study, the particle shape and surface morphology of volcanic scoria powders (ground at different grades) data were analyzed.

# 2 EXPERIMENTAL DATA

### 2.1 Powders Samples

Four volcanic scoria groups according to the color of scoria have been collected. The collected sample was firstly sieved using the 5 mm stainless steel sieve of 20 cm diameter to separate large volcanic scoria (5–100 mm in order) to fine volcanic scoria ( $\leq$ 5 mm). The volcanic scoria sample was performed on the material dried in an open air environment during 24 h and in the oven at 105 °C during 24 h for the removal of moisture in the rocks (Juimo et al, 2016).

The mill process was performed for 20 minutes. Milling sample has been introduced at the same weight for each production. The rotation speed of the mill was about 70 rpm (Bouyahyaoui et al, 2018). Each powder obtained has been described by a twocomponent code designation: the letter reflecting powder color as black (B), dark-red (DR), red (R) and yellow (Y) followed by the 'np' reflecting natural powder or natural pozzolan (Juimo et al, 2017).

### 2.2 Measurement Methods

#### 2.2.1 Gas Pycnometer and Blaine Air Permeability (Blaine Fineness, BF)

In this work, the density of powders was performed on a Gas Pycnometer. This method measures the density by determining the volume of inert gas that can be introduced into a sample chamber of a defined size which contains a known mass of powder. Automatic Gas Pycnometer has long been identified as the instrument of choice to accurately measure the true density of solid materials by employing Archimedes' principle of fluid displacement, and Boyle's Law of gas expansion (Niesel. 1973; EN 196-6, 2010). Helium inert gas, rather than a liquid, is used since it will penetrate even the finest pores and eliminate the influence of surface chemistry. This ensures quick results of the highest accuracy.

The fineness of the grinding was being determined according to the Blaine technique and is indicated as the specific surface (Blaine fineness value). The Blaine Air Permeability apparatus serves exclusively for the determination of the specific surface area ( $S_{SB}$ ) of powders. The Blaine Fineness (BF) value is not a measure of granulometric distribution (Means PSD).

#### 2.2.2 Laser Diffraction (LD)

The granulometry of powders was determined by many methods (sieve analysis, LD, IA, etc.), but the question is how adequately they describe the powder granulometry (Mikli et al, 2001). Mikli et al. (Mikli et al, 2001) reported that the evaluation of the fine powder granulometry (with particle size less than 50 µm) is more difficult and the results of the sieve analysis do not describe adequately the powder granulometry. For this reason, the first method used here to describe powder granulometry is LD. LD which is based on a complex theory of interaction between monochromatic light and individual particles. This involves the detection of the angular distribution of light scattered by a set of monodispersed spherical particles to provide a 'sphere'-equivalent size diameter distribution using a reverse optical scattering-based model calculation (Michel and Courard, 2014).

In LD, the angular distribution of light is measured after passing through an optically dilute dispersion of suspended particles. The LD system determines the PSD based on a volumetric basis. Different optical models are commonly used to build the PSD weighted by apparent volume (volume of an equivalent sphere of diameter D), such as Mie theorybased and Fraunhofer models (Michel and Courard, 2014; Varga et al, 2018).

#### 2.2.3 Image Analysis (IA)

IA has made a decisive breakthrough in the recent years to become a reference technique in the field of combined size and shape analysis of particles (Arvaniti et al, 2015b; Gregoire et al, 2007). The IA is a method for the measurement of particle size and shape distributions. For the measurement of particle size and morphometric characterization, an Occhio 500 Nano image analyzer has been used. The morphology of a powder particle is characterized by shape description (elongation, circularity, solidity, roughness, bluntness (with the calypter), luminance) or quasi-quantitatively, for example, by means of geometrical shape parameters.

The IA is based on the measurement of each particle; the accuracy of a size and shape distribution has to be formulated in number of particles ( $N_P$ ) and not in terms of sample weight or duration of the analysis. The adequate particle number is linked to the shape of the distribution curve and its extension or range (Gregoire et al, 2007). Volcanic scoria powders tested by the IA had respectively: 24,268 particles for Bnp, 32,302 particles for DRnp, 22,562 particles for Rnp and 25,041 particles for Ynp.

### **3 DATA ANALYSIS METHODS**

Data sets obtained by experimental analysis were studied using SPSS software to understand the influence and the correlation of different considerable parameters (factors). The analysis of the individual influence of a given factor in the description of a complex phenomenon, such as the max distance  $(X_{DM})$  or geodesic length  $(X_{LG})$  of the powder particle can lead to erroneous conclusions; for example a given factor could seem extremely relevant when it is not. Slinker and Glantz (Slinker and Glantz, 2008) and Neves et al. (Neves et al, 2018) reported that, a given variable may appear unrelated to the dependent variable when analyzed alone, but may have a strong influence when considered simultaneously with other predictors. To model and identify the main factors that influence the other size parameter descriptors in particle max distance and geodesic length, a multiple linear regression (MLR) analysis is used, which makes if possible examine the simultaneous effects of multiple of independent predictor variables (IPVs) in the variability of the dependent or explained variable (Neves et al, 2018).

Table 1: Definitions of response variables and IPVs in the systems.

Variable/Definition								
Y or Y <sub>i</sub>	Max Distance $(X_{DM})$ , Geodesic length $(X_{LG})$ , Powdering ratio index by Blaine $(Pr_{SB} = N_P/(S_{SB} \times D_S))$ or Powdering ratio index by LD $(Pr_{SL} = N_P/(S_{SL} \times D_S))$ .							
Var.	Definition	Variable	Definition					
<i>x</i> <sub>1</sub>	Inner Diameter $(X_{DI})$	<i>y</i> <sub>1</sub>	Elongation $(E_l)$					
<i>x</i> <sub>2</sub>	Area Diameter $(X_{DA})$	<i>y</i> <sub>2</sub>	Circularity ( $C_c$ )					
<i>x</i> <sub>3</sub>	Width $(W_b)$	<i>y</i> <sub>3</sub>	Solidity $(S_d)$					
<i>x</i> <sub>4</sub>	Length $(L_b)$	<i>y</i> <sub>4</sub>	Roughness $(R_g)$					
<i>x</i> <sub>5</sub>	Max Distance $(X_{DM})$	<i>y</i> <sub>5</sub>	Luminance $(L_m)$					
<i>x</i> <sub>6</sub>	Geodesic length $(X_{LG})$	$y_6$	Bluntness $(B_t)$					

This study also aimed to evaluate the potential relationship between dependent variables (i.e.,  $X_{DM}$ ;  $X_{LG}$ ;  $Pr_{SB}$  or  $Pr_{SL}$ ) and input variables (i.e.,  $X_{DI}$ ;  $X_{DA}$ ;  $W_b$ ;  $L_b$ ;  $X_{DM}$ ;  $X_{LG}$ ;  $E_l$ ;  $C_c$ ;  $S_d$ ;  $R_g$ ;  $L_m$ ;  $B_t$ ) by applying statistical models. The independent variables  $Pr_{SB}$  and  $Pr_{SL}$  expresses by  $N_P/(S_{SB} \times D_S)$  and  $N_P/(S_{SL} \times D_S)$ , and represent powdering ratio index of powders by BF and LD respectively.

The explanatory variables included in models are :  $X_{DI}$ ;  $X_{DA}$ ;  $W_b$ ;  $L_b$ ;  $X_{DM}$ ;  $X_{LG}$ ;  $E_l$ ;  $C_c$ ;  $S_d$ ;  $R_g$ ;  $L_m$  and  $B_t$ . Besides the conventional linear regression model, introduced as Model 1(with 4 IPVs) and Model 2 (with 5 IPVs) in Equation (1) based on the linear regression model provide by Neves et al. (Neves et al, 2018) and Jin et al. (Jin et al, 2018).

$$Y = f(x_i) \rightarrow Y = \alpha_0 + \sum_{i=1}^n \alpha_i x_i + \varepsilon = \alpha_0 + \alpha_1 x_1 + \alpha_2 x_2 + \dots + \alpha_n x_n + \varepsilon$$
(1)

where Y represents the dependent variable (also called response variable, output, endogenous or explained),  $\alpha_0$ ,  $\alpha_1$ , . . .,  $\alpha_k$  the regression coefficients,  $x_1, x_2, \ldots, x_k$  the IPVs (Table I) and  $\epsilon$  the random errors of the model.

Equat	ion	IPVs used to predict Max IPVs used to predict IPVs used to predict IPVs used to predict								
/Model n°		Distance $(X_{DM})$	Geodesic length $(X_{LG})$	Powdering ratio index by Blaine $(Pr_{SB} = N_P / (S_{SB} \times D_S))$	Powdering ratio index by LD ( $Pr_{SL} = N_P/(S_{SL} \times D_S)$ )					
Eq.	1	$X_{DI}, X_{DA}, W_b, L_b$	-	-	-					
(1)	2	$X_{DI}, X_{DA}, W_b, L_b, X_{LG}$	$X_{DI}, X_{DA}, W_b, L_b, X_{DM}$	-	-					
	3	$X_{DI}, X_{DI} \times E_l, X_{DI} \times C_c, X_{DI} \times R_g, X_{DI} \times S_d, X_{DI} \times L_m, X_{DI} \times B_t$								
	4	$X_{DA}, X_{DA} \times E_l, X_{DA} \times C_c, X_{DA} \times R_g, X_{DA} \times S_d, X_{DA} \times L_m, X_{DA} \times B_t$								
Eq. (2)	5	$W_b \text{ , } W_b \times E_l \text{ , } W_b \times C_c \text{ , } W_b \times R_g \text{ , } W_b \times S_d \text{ , } W_b \times L_m \text{ , } W_b \times B_t$								
	6	$L_b$ , $L_b \times E_l$ , $L_b \times C_c$ , $L_b \times R_g$ , $L_b \times S_d$ , $L_b \times L_m$ , $L_b \times B_t$								
	7	7 - $X_{DM}, X_{DM} \times E_l, X_{DM} \times C_c, X_{DM} \times R_g, X_{DM} \times S_d, X_{DM} \times L_m, X_{DM} \times B_t$								
	8	$\begin{array}{c} X_{LG} , X_{LG} \times E_l , X_{LG} \times \\ C_c , X_{LG} \times R_g , X_{LG} \times \\ S_d , X_{LG} \times L_m , X_{LG} \times B_t \end{array}$	-	$X_{LG}, X_{LG} \times E_l, X_{LG} \times C_c, X_{LG}$ $S_d, X_{LG} \times L_m, X_{LG} \times B_t$	$X_{LG}  imes R_g$ , $X_{LG}  imes$					

Table 2: Description of the multiple linear regression model.

The regression equation given by Equation (1) gives the value predicted for the dependent variable according to the IPVs included in the model, which lies on the best-fit regression plane, which represents the multidimensional generalization of a line (Slinker and Glantz, 2008; Neves et al, 2018).

In this research we also proposed alternative nonlinear models to improve the determination coefficients when predicting dependent variables (Model 1 & 2: Multi-linear regression analysis).

These models range from Model 3 to Model 8 in Equation (2), where  $i = 1, \dots, 6$  denotes the number of IPVs concerning particle size descriptors. The analysis of the interactions between size and shape parameters in the description the max distance or geodesic length of the powder particle, a MLR analysis is used, which allows examining the simultaneous effects of multiple IPVs in the variability of the dependent or explained variable with variables interact.

The statistical relationship between the dependent variable  $Y_i$  and the multiple IPVs  $x_i$  and  $y_k$  is given by Equation (2) (Model 3 to 8: Non-linear model involving variables interactions).

$$Y_{i} = f(x_{i}, y_{j}) \rightarrow Y_{i} = \beta_{0} + \sum_{j=1}^{k} \beta_{j} x_{i} y_{j} +$$

$$\varepsilon = \beta_{0} + \beta_{1} x_{i} y_{1} + \beta_{2} x_{i} y_{2} + \cdots$$

$$+ \beta_{k} x_{i} y_{k} + \epsilon$$

$$(2)$$

where  $Y_i$  represents the dependent variable (also called response variable, output, endogenous or explained,  $i = 1, \dots, n$ ),  $\beta_0$ ,  $\beta_1$ , . . . ,  $\beta_k$  the regression coefficients,  $x_i$  and  $y_1, x_2, \dots, y_k$  the independent variables (Table 1) and  $\varepsilon$  the random errors of the model.

The regression equation given by Equation (2) gives the value predicted for the dependent variable according to the IPVs included in the model which lies on the best-fit regression plane that represents the multidimensional generalization of a line (Slinker and Glantz, 2008; Neves et al, 2018).

Among the k independent predictor variables (IPVs), some may have more significant effects on the target response variable than others as reported by Jin et al. (Jin et al, 2018). In the same way, the t-test of correlation analysis was used to determine the significance regarding the effect of each IPV on the response variable in this study. There is a p-value corresponding to each t-value for an IPV. At the 95% confidence level, a p-value lower than 0.05 would indicate that this selected IPV makes a significant contribution to the response variable. In contrast, IPVs with p-values higher than 0.05 are those without significant contributions. A possible reason why some IPVs had higher significance than others was the strong internal correlation among IPVs, which caused redundancies. Therefore, the regression

analysis could be redone by removing the redundant IPVs, shortening the equation to include only significant IPVs. Target models, response variables and various IPVs using input systems are defined in Table 1 and Table 2.



Figure 1: Summary of production process and main testing data of powders.

#### 4 RESULTS AND DISCUSSION

### 4.1 Principal Properties

The powders obtained have a density between 2.8 and 3.1 g/cm<sup>3</sup> and SSA Blaine between 3,500 and 5,300 cm<sup>2</sup>/g, which are comparable to ordinary Portland cement fineness ((Bouyahyaoui et al, 2018; Juimo et al, 2017).

By LD, mean particle diameter (Dmed), mean particle diameter of 10% of particles D(10), median particle diameter D(50) and mean particle diameter of 90% of particles D(90) were measured to evaluate the efficiency of the milling process. Using the PSD data obtain by LD and Equations (1)-(2),  $S_{SL}$  evaluated are ranging between 4,400 to 6,000 cm<sup>2</sup>/g.  $S_{SL}$  value obtains by this method for each powder is always higher, that is about 4% to 25% than  $S_{SB}$  obtain by BF (Figure 1). PSDs of powders were evaluated by using the LD and IA (Figure 1). In the LD technique, the angular distribution of light is measured after passing through an optically dilute dispersion of suspended particles. This technique is widely used in dust and mineral industry with water and dispersive agent to a special cell where the laser light is sent (Felekoglu, 2009; Orhan et al, 2004).

The inscribed disk diameter ( $X_{DI}$  or  $X_{DA}$ ) of each particle is calculated in real time to build PSD curves weighted by apparent volume (Gregoire et al, 2007), making the assumption that particles have identical flatness ratios, whatever their size (Michel and Courard, 2014). Area diameter of particles was used to plot PSD curve obtained by IA. The PSD profile shows a negligible difference in the results by the two methods (Abazarpoor et al, 2017). The main reasons for differences between two PSD methods are as follows: the considerate particle diameter by each measurement process, the different shapes of the particles; better insight into particles using the IA method; insufficient dispersion of fine particles; fine particles adhering to the bigger particles. LD and 2D projection image by the IA are commonly used the PSD measurement techniques, but the results may not be representative of the strongly true physical dimensions of the particles (Califice et al, 2013).

## 4.2 Particle Morphology Analysis

More than 50 images of powder particles were identified. The particle morphology was found to provide reasonable accuracy for estimating the particle sizes of highly porous particles, where the distinction between inter-particle and intra-particle porosity was made. This important comment concerning inter-particle and intra-particle porosity has been also reported by Klemm and Wiggins (Klemm and Wiggins, 2017).

#### 4.2.1 Particle Morphology: Size Parameters Distribution

Figure 2 shows the general identification of particles according to their inner diameter and area diameter. About 25% of Bnp particles, 25% of Ynp particles, 25% of DRnp particles, 25% of Bnp and 5% of Bnp particles have the same area diameter like respectively a particle n°1, n°2, n°3, n°4 and n°5 as

showing in Figure 2. In the same way, about 5% of DRnp particles, 5% of Bnp particles, 6% of Rnp particles, 6% of Ynp and 25% of Ynp particles have the same area diameter like respectively a particle  $n^{\circ}1$ ,  $n^{\circ}2$ ,  $n^{\circ}3$ ,  $n^{\circ}4$  and  $n^{\circ}5$  as showing in Figure 2.



Figure 2: Identification of particles based on their inner diameter and area diameter.

Particles who have a high inner diameter and area diameter are from DRnp powder and Particles who present a very few inner diameter and area diameter are from Rnp and Ynp powders.



Figure 3: Relation between (a) inner and area diameter, (b) width and length and (c) max distance and geodesic length consider all powders.

Figure 3a shows that for all data obtained for all powders, inner diameter and area diameter are well related with a coefficient of correlation up to 0.99.

Figure 4 shows the general identification of particles according to their inner diameter and area diameter. About 25% of Bnp particles, 25% of DRnp particles, 25% of Bnp particles, 6% of Ynp and 5% of Bnp particles have the same width as particles n°11, n°12, n°13, n°9 and n°7 respectively as shown in Figure 4.

In the same way, about 5% of DRnp particles, 5% of Rnp particles, 25% of Rnp particles, 25% of Rnp and 25% of Ynp particles have the same length as particles n°6, n°14, n°8, n°15 and n°16 respectively as also shown in Figure 4. Particles that have a higher width are from DRnp powder and those that present a higher length are from Ynp powder. Particles that present a very few width and length are from Rnp and Ynp powders. Figure 3b shows that for all data

obtained for all powders, width and length are well related with a coefficient of correlation up to 0.98.



Figure 4: Identification of particles based on their width and length.

Figure 5 shows the general identification of particles according to their max distance and geodesic length. About 25% of Bnp particles, 25% of DRnp particles, 25% of Bnp particles, 5% of Rnp and 5% of DRnp particles have the same max distance as particles  $n^{o}11$ ,  $n^{o}17$ ,  $n^{o}18$ ,  $n^{o}14$  and  $n^{o}6$  respectively as shown in Figure 5. In the same way, about 5% of Ynp particles, 5% of Rnp and 25% of Ynp particles have the same geodesic length as particles  $n^{o}19$ ,  $n^{o}20$ ,  $n^{o}21$ ,  $n^{o}22$  and  $n^{o}23$  respectively as also shown in Figure 5.



Figure 5: Identification of particles based on their max distance and geodesic length.

Particles that have a higher max distance are from DRnp and Ynp powders and whose who present a higher geodesic length are from DRnp powder. Particles that present a very few max distance and geodesic length are from Rnp and Ynp powders.

Figure 3c shows that for all data obtained for all powders, max distance and geodesic length are well related with a coefficient of correlation up to 0.97.

#### 4.2.2 Particle Morphology: Shape Parameters Distribution

Figure 6 shows the general identification of particles according to their elongation and circularity. About 4% of DRnp particles, 9% of Bnp particles, 25% of Ynp particles, 25% of DRnp and 6% of Ynp particles have the same circularity as particles n°6, n°24, n°25, n°26 and n°27 respectively as shown in Figure 6.



Figure 6: Identification of particles based on their elongation and circularity.

In the same way, about 5% of Ynp particles, 5% of Rnp particles, 25% of DRnp particles, 25% of Bnp and 25% of DRnp particles have the same elongation as particles n°19, n°14, n°28, n°11 and n°17 respectively as also shown in Figure 6. Particles that have a higher elongation are from Rnp and Ynp powders and those that present a higher circularity are from Rnp and Ynp powders. Particles that present a very few elongation and circularity are from Bnp and DRnp powders.

Figure 7 shows the general identification of particles according to their roughness and solidity. About 6% of Bnp particles, 6% of DRnp particles, 5% of DRnp particles, 5% of Rnp and 6% of Ynp particles have the same roughness as particles  $n^{\circ}29$ ,  $n^{\circ}30$ ,  $n^{\circ}31$ ,  $n^{\circ}32$  and  $n^{\circ}19$  respectively as shown in Figure 7.

In the same way, about 25% of Rnp particles, 25% of DRnp particles, 25% of Ynp particles, 25% of Bnp and 25% of DRnp particles have the same solidity as particles n°33, n°17, n°25, n°7 and n°6 respectively

as also shown in Figure 7. Particles that have a higher roughness are from Ynp powder. Particles that present a very few roughnesses are also from Ynp powder. These powder particles have in general a solidity value equal to 1.0. This means that these particles from volcanic scoria have a higher solidity.



Figure 7: Identification of particles based on their roughness and solidity.

Figure 8 shows the general identification of particles according to their luminance and bluntness. About 4% of DRnp particles, 5% of Bnp particles, 25% of Rnp particles, 25% of Ynp and 5% of Rnp particles have the same bluntness as particles n°34, n°35, n°36, n°16 and n°37 respectively as shown in Figure 8.



Figure 8: Identification of particles based on their luminance and bluntness.

In the same way, about 5% of DRnp particles, 5% of Rnp particles, 5% of Bnp particles, 9% of Ynp and 25% of Bnp particles have the same luminance as particles n°28, n°38, n°39 and n°40 respectively

as also shown in Figure 8. Particles that have a higher luminance are from DRnp powder. Particles that present a very few luminance are from Rnp and Bnp powders.

#### 4.3 Study the Correlation Between Several Parameters

In this study, the two major input systems within volcanic scoria powder particle morphology (i.e., size and shape input systems) were compared for their accuracy in predicting considered dependent variable. In addition, the effect of number of particle projections  $(N_P)$  on the variables obtained through IA is investigated.

The bestfit models were identified under each input system. By removing significantly correlated IPVs within each input system, the regression modelling process was rerun by shortlisting (Jin et al, 2018).

Figure 9 presents the summary of measurement values for size and shape parameters of powder sample identifying the variables considered in this study. These data are used for the definition of several models, to predict the considerable dependent variable. These values have obtained the consideration of 24,268, 32,302, 22,562 and 25,041 particles for Bnp, DRnp, Rnp and Ynp respectively. For all size parameters, the value is down to 500 μm for all powders.

The regression analysis was conducted based on the proposed models for input systems, respectively. The reliability of these models was compared, and the best-fit model was identified. Table 3 displays the corresponding  $R^2$  values for all predictions. The summary of models is shown in Table 3 where the statistical coefficients analyzed are presented to evaluate the validity of the regression model. The model proposed for samples leads a correlation coefficient (R) of 0.810 and a determination coefficient (R<sup>2</sup>) of 0.779, thus revealing a very strong correlation between the values predicted by the model and the values observed in the dataset.

Table 3 shows also the analysis of variance (ANOVA) of models. The ANOVA table reveals an F value (Fisher-Snedecor test) of models, which is considerably higher than the critical value of F, for a level of significance of 5%. Moreover, the significance value of the model is practically null, thus lower than the p-value adopted as significance level (5%). The results obtained reveal that all the independent variables considered are statistically significant in explaining the dependent variable.

As shown in Table 3, input systems led to highly consistent R<sup>2</sup> values (up to 0.919) from Models 1 to 8 for predicting  $X_{DM}$  and  $X_{LG}$ , meaning similar prediction accuracy. Model 4 (the mixed model using

size/shape as the RRV) achieved the consistently high  $R^2$  values for all the four predicted variables ( $X_{DM}$ ,  $X_{LG}$ ,  $Pr_{SB}$  or  $Pr_{SL}$ ).



Figure 9: Summary of measurement values for size and shape parameters of powders.

All of the corresponding  $R^2$  values in the 25 scenarios are within the reasonable range (i.e., 0.810–0.998). Model 1 also achieved the highest  $R^2$  value for the prediction of  $X_{DM}$  in both systems (0.998 for Multi-linear regression analysis and 0.979 for Non-linear model involving variables interactions).

In the  $Pr_{SB}$  or  $Pr_{SL}$  regression analysis, Model 6 (the non-linear approach) represents the best-fit model by achieving even higher accuracy than others, the highest based on both input systems.

The remaining mixed models had relatively lower  $R^2$  values for both input systems. The  $R^2$  values resulting from the best-fit non-linear and mixed regression models in this research (ranging from 0.810–0.998) are significantly higher than the values generated from previous studies adopting linear methods. This can be seen in Table 3.

According to these correlation and ANOVA coefficients, model 2, model 5 and model 6 are the three best models to predict max distance and geodesic length and the best model to predict Powdering ratio index by Blaine and by LD is the model 6 as indicated in bold in Table 3.

The linear regression coefficients ( $\alpha_i$  or  $\beta_i$ ) of the proposed models were determinate. All the independent variables included in the model are statistically relevant in the description of the variability of the dependent variable, showing a significance value lower than the p-value (5%). The linear regression coefficients of model present a significance value lower than the p-value (5%), indicating that all the independent variables are statistically relevant in the description of the dependent response n coefficient obtained from this test technique (Table 4). These significance values are marked in green and the models selected on this basis are also marked in bold in Table 4. According to these p-values, model 2 and model 5 are the two best models to predict max distance and geodesic length and the best model to predict Powdering ratio index by Blaine and by LD is the model 6 as indicated in bold in Table 4.

Once the statistical relevance of models is confirmed, Table 5 presents the mathematical formulation that makes rating estimation of each dependent response possible.

Table 3: Summary of the multiple linear regression analysis results (In this table, \*Analysis of variance of the model (ANOVA), \*\*Square of the mean square error (RMSE))

Paran	neter			Co	ANOVA*				
Eq.	Mo	del nº	R $R^2$ $R^2ad$ .		RMSE**	F value	p value		
uc	1 X <sub>DM</sub>		0.998	0.996	0.996	3.868045369	2436.723	0.000	
Equation (1)	2 X <sub>DM</sub>		0.999	0.998	0.997	2.963935818	3325.711	0.000	
й		X <sub>LG</sub>	0.972	0.944	0.944	34.390131493	128.921	0.000	
	3	X <sub>DM</sub>	0.942	0.888	0.866	21.326295389	40.846	0.000	
		X <sub>LG</sub>	0.959	0.919	0.904	42.540114280	58.587	0.000	
		Pr <sub>sb</sub>	0.951	0.904	0.885	0.286212210	48.326	0.000	
		Pr <sub>sL</sub>	0.945	0.892	0.871	0.244277238	42.594	0.000	
	4	X <sub>DM</sub>	0.968	0.936	0.924	16.097413373	75.576	0.000	
		X <sub>LG</sub>	0.969	0.939	0.927	36.948598108	79.335	0.000	
		Pr <sub>sb</sub>	0.944	0.891	0.870	0.304327341	42.150	0.000	
		Pr <sub>sL</sub>	0.946	0.896	0.876	0.240259398	44.204	0.000	
	5	X <sub>DM</sub>	0.989	0.979	0.974	9.349541278	234.136	0.000	
		X <sub>LG</sub>	0.980	0.960	0.952	29.887883900	123.964	0.000	
Equation (2)		Pr <sub>sb</sub>	0.942	0.888	0.866	0.308774263	40.798	0.000	
guati		Pr <sub>sL</sub>	0.944	0.892	0.871	0.244995796	42.314	0.000	
щ	6	X <sub>DM</sub>	0.998	0.996	0.996	3.787558166	1452.888	0.000	
		X <sub>LG</sub>	0.979	0.959	0.951	30.442169551	119.306	0.000	
		Pr <sub>SB</sub>	0.931	0.866	0.840	0.337897319	33.220	0.000	
		Pr <sub>sL</sub>	0.936	0.876	0.852	0.261645598	36.467	0.000	
	7	X <sub>LG</sub>	0.973	0.947	0.937	34.388965646	92.379	0.000	
		Pr <sub>sB</sub>	0.930	0.864	0.838	0.340304620	32.679	0.000	
		Pr <sub>sL</sub>	0.935	0.873	0.849	0.264888669	35.454	0.000	
	8	X <sub>DM</sub>	0.966	0.934	0.923	16.211425615	86.685	0.000	
		Pr <sub>sb</sub>	0.900	0.810	0.779	0.396643132	26.314	0.000	
		Pr <sub>SL</sub>	0.903	0.815	0.785	0.315815860	27.153	0.000	

According to these equations with higher correlation (Table 5), including main characteristics of powders: the particle size, particle shape and technological properties of powders (density, surface area, etc.). It is demonstrated that using powders, as well as the potential areas of their application, strongly depends on these characteristics. Dimensionless relationships between particle size and particle shape can be determined theoretically for simplified, but realistic, powder particle geometries. These relationships have important implications for the interpretation of shape data, and, more fundamentally, for the selection of grain size(s) for analysis.

# **5** CONCLUSIONS

This study showed that the size estimation of particulate material is a complicated matter. The results highlight the fact that particle size distributions may not be unique. Different techniques can give a large range of different parameters which need to be interpreted correctly. The choice of the parameters also depends on the purpose of the research. It is shown that particle shape analysis that includes the full range of available grain sizes can contribute not only measurements of particle size and shape, but also information on size-dependent densities and specific surface area.

Based on the analysis of particle characteristics, design of experiment, and analysis of variance (ANOVA), it can be concluded that: good correlation was found between the specific surface area measured by Blaine Permeability Tester and calculated from the LD and the IA data.

Thus, based on these conclusions, it appears that the density, specific surface area, granulometry and, morphology of volcanic scoria powders may be efficiently estimated from complementary techniques. This description is absolutely needed for understanding particles' behavior in contact with water when used in cementitious materials.

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Model	n°	Const.	X <sub>DI</sub>	X <sub>DA</sub>	W <sub>b</sub>	L <sub>b</sub>	X <sub>DM</sub>	X <sub>LG</sub>	$X_{DI} \times E_I$	$X_{DI} \times C_c$	$X_{DI} \times R_{q}$	$W_b \times S_d$	$W_b \times L_m$	$W_b \times B_t$
X <sub>DM</sub>	1	0.842	0.226	0.610	0.864	0.000	х	х	x	x	x	x	x	x
X <sub>DM</sub>	2	0.121	0.001	0.304	0.107	0.000	x	0.000	x	x	x	x	x	x
X <sub>LG</sub>		0.008	0.000	0.030	0.006	0.000	0.000	x	x	x	x	x	x	x
X <sub>DM</sub>	3	0.365	x	0.120	x	х	x	х	0.001	0.946	0.038	0.199	0.442	0.203
$X_{LG}$		0.289	x	0.046	х	х	x	х	0.969	0.796	0.903	0.034	0.355	0.000
Pr <sub>SB</sub>		0.279	x	0.405	x	x	x	x	0.584	0.261	0.543	0.234	0.155	0.009
Pr <sub>SL</sub>		0.160	x	0.287	х	х	x	х	0.863	0.198	0.772	0.159	0.109	0.002
Model	4	Const.	X <sub>DI</sub>	X <sub>DA</sub>	W <sub>b</sub>	$L_b$	X <sub>DM</sub>	X <sub>LG</sub>	$X_{DA} \times E_l$	$X_{DA} \times C_c$	$\begin{array}{c} X_{DA} \\ \times R_g \end{array}$	$\begin{array}{c} X_{DA} \\ \times S_d \end{array}$	$\begin{array}{c} X_{DA} \\ \times L_m \end{array}$	$X_{DA} \times B_{t}$
X <sub>DM</sub>		0.365	x	0.120	х	х	x	х	0.001	0.946	0.038	0.199	0.442	0.203
$X_{LG}$		0.289	x	0.046	x	x	x	x	0.969	0.796	0.903	0.034	0.355	0.000
Pr <sub>SB</sub>		0.279	x	0.405	x	x	x	x	0.584	0.261	0.543	0.234	0.155	0.009
Pr <sub>SL</sub>		0.160	x	0.287	x	x	x	х	0.863	0.198	0.772	0.159	0.109	0.002
Model	5	Const.	X <sub>DI</sub>	X <sub>DA</sub>	W <sub>b</sub>	$L_b$	X <sub>DM</sub>	X <sub>LG</sub>	$W_b \times E_l$	$W_b \times C_c$	$W_b \times R_g$	$W_b \times S_d$	$W_b \times L_m$	$W_b \times B$
X <sub>DM</sub>		0.110	x	x	0.094	x	x	x	0.000	0.265	0.000	0.042	0.000	0.66
X <sub>LG</sub>		0.748	x	x	0.169	x	x	x	0.000	0.757	0.000	0.105	0.907	0.000
Pr <sub>SB</sub>		0.334	x	х	0. 605	x	x	x	0.885	0.267	0.944	0.358	0.023	0.002
Pr <sub>SL</sub>		0.118	x	х	0.249	x	x	х	0.870	0.182	0.462	0.130	0.001	0.00
Model	6	Const.	X <sub>DI</sub>	X <sub>DA</sub>	W <sub>b</sub>	L <sub>b</sub>	X <sub>DM</sub>	X <sub>LG</sub>	$L_b \times E_l$	$L_b \times C_c$	$\begin{array}{c} L_b \\ \times R_g \end{array}$	$L_b \times S_d$	$L_b \times L_m$	$\begin{array}{c} L_b \\ \times B \end{array}$
$X_{DM}$		0.519	x	х	х	0.966	x	х	0.908	0.386	0.330	0.313	0.400	0.384
$X_{LG}$		0.783	х	х	x	0.261	x	x	0.001	0.952	0.084	0.185	0.336	0.000
Pr <sub>sb</sub>		0.035	x	x	x	0.070	x	x	0.041	0.246	0.523	0.042	0.510	0.04
Pr <sub>sL</sub>		0.012	x	x	x	0.028	x	x	0.091	0.183	0.533	0.017	0.260	0.017
Model	7	Const.	X <sub>DI</sub>	$X_{DA}$	W <sub>b</sub>	$L_b$	X <sub>DM</sub>	X <sub>LG</sub>	$X_{DM} \times E_l$	$\begin{array}{c} X_{DM} \\ \times C_c \end{array}$	$\begin{array}{c} X_{DM} \\ \times R_g \end{array}$	$\begin{array}{c} X_{DM} \\ \times S_d \end{array}$	$X_{DM} \times L_m$	$X_{DM} \times B_1$
$X_{LG}$		0.906	х	х	x	x	0.281	х	0.002	0.931	0.061	0.208	0.603	0.000
Pr <sub>SB</sub>		0.037	x	х	х	x	0.092	х	0.035	0.325	0.349	0.056	0.371	0.075
Pr <sub>SL</sub>		0.013	x	x	x	x	0.040	x	0.078	0.255	0.352	0.023	0.176	0.03
Model	8	Const.	X <sub>DI</sub>	X <sub>DA</sub>	W <sub>b</sub>	L <sub>b</sub>	X <sub>DM</sub>	X <sub>LG</sub>	$\begin{array}{c} X_{LG} \\ \times E_l \end{array}$	$\begin{array}{c} X_{LG} \\ \times C_c \end{array}$	$\begin{array}{c} X_{LG} \\ \times R_g \end{array}$	$\begin{array}{c} X_{LG} \\ \times S_d \end{array}$	$\begin{array}{c} X_{LG} \\ \times L_m \end{array}$	$\begin{array}{c} X_{LG} \\ \times B \end{array}$
X <sub>DM</sub>		0.399	x	x	x	x	x	0.076	0.010	0.111	0.136	xx	0.390	0.00
Pr <sub>SB</sub>		0.182	х	х	x	x	x	0.127	0.939	0.021	0.570	xx	0.499	0.00
Pr <sub>SL</sub>		0.122	x	х	х	х	x	0.160	0.585	0.011	0.460	xx	0.351	0.000

Table 4: p-value (In this table, x : non-considered variable, xx : excluded variable).

Model n°	Equations	R <sup>2</sup>
Model 2	$X_{DM} = -1.167 + 0.435 X_{DI} + 0.281 X_{DA} - 0.501 W_b + 1.043 L_b - 0.056 X_{LG}$	0.998
Wodel 2	$X_{LG} = -22.528 + 6.003 X_{DI} + 6.718 X_{DA} - 9.542 W_b + 8.240 L_b - 7.590 X_{DM}$	0.944
Model 5	$ \begin{array}{l} X_{DM} = 6.306 - 4.455 W_b \ - \ 1.989 W_b \times E_l + 0.827 W_b \times C_c + 4.877 W_b \times R_g + 5.815 W_b \times S_d - 1.377 W_b \times L_m + 0.157 W_b \times B_t \end{array} $	0.979
	$ \begin{array}{l} \overline{X_{LG}} = -3.989 + 11.619 W_b - 6.019 W_b \times E_l + 0.727 W_b \times C_c + \\ 8.110 W_b \times R_g - 14.650 W_b \times S_d - 0.053 W_b \times L_m + 7.069 W_b \times B_t \end{array} $	0.960
Model 6	$Pr_{SB} = 0.302 - 0.145L_{b} - 0.031L_{b} \times E_{l} + 0.024L_{b} \times C_{c} + 0.025L_{b} \times R_{g} + 0.175L_{b} \times S_{d} - 0.006L_{b} \times L_{m} - 0.021L_{b} \times B_{t}$	0.866
	$ Pr_{SL} = 0.282 - 0.137L_b - 0.019L_b \times E_l + 0.021L_b \times C_c + 0.019L_b \times R_g + 0.162L_b \times S_d - 0.008L_b \times L_m - 0.020L_b \times B_t $	0.876

Table 5: Equations of efficient models identified.